



Introduction to Fire Dynamics Tools (NUREG-1805)

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Agenda:

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Introduction

- The U.S. Nuclear Regulatory Commission (NRC) created the Fire Dynamics Tools (FDTs) quantitative methods, to help out in performing Fire Hazard Analyses (FHAs) known as NUREG 1805.
- This methodology has been implemented by populated *Excel* spreadsheets.
- The dynamic nature of fire is a quantitative and mathematically complex subject. It combines physics, chemistry, mathematics, and engineering principles.
- The objective of NUREG 1805 is to provide first-order calculations of potential fire scenarios at nuclear power plants.



Introduction

List of Fire Dynamics Tools:

| FDT ^{s*} | Chapter and Related Calculation Method(s) |
|---|--|
| *indicated revised spreadsheet 02.1_Temperature_NV_Sup1.xls 02.2_Temperature_FV_Sup1.xls* 02.3_Temperature_CC._Sup1.xls* | Chapter 2. Predicting Hot Gas Layer Temperature and Smoke Layer Height in a Room Fire with Natural and Forced Ventilation Method of McCaffrey, Quintiere, and Harkleroad (MQH) <ul style="list-style-type: none">Natural Ventilation Method of Foote, Pagni, and Alvares (FPA) <ul style="list-style-type: none">Forced Ventilation Method of Deal and Beyler <ul style="list-style-type: none">Forced Ventilation Method of Beyler <ul style="list-style-type: none">Fire in a Compartment with a Door Closed but with Sufficient Leaks to Prevent Pressure Buildup; Leakage is Ignored |



Introduction

List of Fire Dynamics Tools:

| FDT ^{s*} | Chapter and Related Calculation Method(s) |
|--|--|
| *indicated revised spreadsheet | |
| 03_HRR_Flame_Height_Burning_Duration_Calculation_Sup1.xls* | Chapter 3. Estimating Burning Characteristics of Liquid Pool Fire, Heat Release Rate, Burning Duration and Flame Height |
| 04_Flame_Height_Calculations_Sup1.xls | Chapter 4. Estimating Wall Fire Flame Height, Line Fire Flame Height Against the Wall, and Corner Fire Flame Height |
| 05.1_Heat_Flux_Calculations_Wind_Free_Sup1.xls 05.2_Heat_Flux_Calculations_Wind_Sup1.xls* 05.3_Thermal_Radiation_From_Hydrocarbon_Fireballs_Sup1.xls | Chapter 5. Estimating Radiant Heat Flux from Fire to a Target Fuel <i>Wind-Free Condition</i> <ul style="list-style-type: none"> • Point Source Radiation Model (Target at Ground Level) • Solid Flame Radiation Model (Target at Ground Level) • Solid Flame Radiation Model (Target Above Ground Level) <i>Presence of Wind</i> <ul style="list-style-type: none"> • Solid Flame Radiation Model (Target at Ground Level) • Solid Flame Radiation Model (Target Above Ground Level) Estimating Thermal Radiation from Hydrocarbon Fireballs |



Introduction

List of Fire Dynamics Tools:

| | |
|--|---|
| 06_Ignition_Time_Calculations_Sup1.xls | <p>Chapter 6. Estimating the Ignition Time of a Target Fuel Exposed to a Constant Radiative Heat Flux</p> <ul style="list-style-type: none">• Method of Estimating Piloted Ignition Time of Solid Materials Under Radiant Exposures Method of (1) Mikkola and Wichman, (2) Quintiere and Harkleroad, and (3) Janssens• Method of Estimating Piloted Ignition Time of Solid Materials Under Radiant Exposures Method of Toal, Silcock and Shields• Method of Estimating Piloted Ignition Time of Solid Materials Under Radiant Exposures Method of Tewarson |
| 07_Cable_HRR_Calculations_Sup1.xls | <p>Chapter 7. Estimating Full-Scale Heat Release Rate of a Cable Tray Fire</p> |
| 08_Burning_Duration_Soild_Sup1.xls | <p>Chapter 8. Estimating Burning Duration of Solid Combustibles</p> |



Introduction

List of Fire Dynamics Tools:

| | |
|--|---|
| 09_Plume_Temperature_Calculations_Sup1.xls | Chapter 9. Estimating Centerline Temperature of a Buoyant Fire Plume |
| 10_Detector_Activation_Time_Sup1.xls* | Estimating Detector Response Time Chapter 10. Estimating Sprinkler Response Time Chapter 11. Estimating Smoke Detector Response Time Chapter 12. Estimating Heat Detector Response Time |
| 13_Compartment_Flashover_Calculations_Sup1.xls | Chapter 13. Predicting Compartment Flashover <ul style="list-style-type: none"> • Compartment Post-Flashover Temperature: Method of Law • Minimum Heat Release Rate Required to Compartment Flashover: Method of (1) McCaffrey, Quintiere, and Harkleroad (MQH); (2) Babrauskas; and (3) Thomas |
| 14_Compartment_Over_Pressure_Calculations_Sup1.xls | Chapter 14. Estimating Pressure Rise Attributable to a Fire in a Closed Compartment |
| 15_Explosion_Calculations_Sup1.xls | Chapter 15. Estimating the Pressure Increase and Explosive Energy Release Associated with Explosions |
| 16_Battery_Room_Flammable_Gas_Conc_Sup1.xls* | Chapter 16. Calculating the Rate of Hydrogen Gas Generation in Battery Rooms <ul style="list-style-type: none"> • Method of Estimating Hydrogen Gas Generation Rate in Battery Rooms • Method of Estimating Flammable Gas and Vapor Concentration Buildup in Enclosed Spaces • Method of Estimating Flammable Gas and Vapor Concentration Buildup Time in Enclosed Spaces |



Introduction

List of Fire Dynamics Tools:

| | |
|---|---|
| <p>17.1_FR_Beams_Columns_Substitution_Correlation_Sup1.xls*</p> <p>17.2_FR_Beams_Columns_Quasi_Steady_State_Spray_Insulated_Sup1.xls*</p> <p>17.3_FR_Beams_Columns_Quasi_Steady_State_Board_Insulated_Sup1.xls*</p> <p>17.4_FR_Beams_Columns_Quasi_Steady_State_Uninsulated_Sup1.xls*</p> | <p>Chapter 17. Calculating the Fire Resistance of Structural Steel Members</p> <ul style="list-style-type: none">• Empirical Correlations• Beam Substitution Correlation (Spray-Applied Materials)• Column Substitution Correlation (Spray-Applied Materials)• Heat Transfer Analysis using Numerical Methods Protected Steel Beams and Columns (Spray-Applied)• Heat Transfer Analysis using Numerical Methods Protected Steel Beams and Columns (Board Materials)• Heat Transfer Analysis using Numerical Methods Unprotected Steel Beams and Columns |
| <p>18_Visibility_Through_Smoke_Sup1.xls</p> | <p>Chapter 18. Estimating Visibility Through Smoke</p> |
| <p>19_THIEF_of_Cables_Calculations_Sup1.xls</p> | <p>Chapter 19. Estimating the Thermally-Induced Electrical Failure (THIEF) of Cables</p> |



Introduction

Advantages of NUREG 1805:

- User-friendly, Pre-programmed Excel spreadsheets based on fire dynamics equation/correlations.
- Quick application of fire dynamics principles.
- Protected spreadsheets prevents tampering.
- Automatic unit conversion.
- Fire materials properties data for generally used in nuclear power plants programmed within each spreadsheet.
- Pull-down menus decreases input errors.
- Spreadsheets are available in English and SI Units.



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NUREG 1805 Example

Room 135 contains switchgear equipment as well as three transformers contained in a fenced section of the room. The room has approximate LxWxH dimensions of 19 x 20 x 12 ft (5.8 x 6.1 x 3.6 m) [8.2.1]. The room has no mechanical ventilation but is provided with a 18"x12" vent for natural ventilation. The walls and roof of the room are of wooden construction. It should be noted as well there is no rooms or spaces above the ceiling.

The combustible material observed in the room is comprised of the electrical equipment and three cable spools. There were no other large sources of combustibles present within the room. Ignition sources in this room consist of the electrical equipment present as well as two heaters suspended from the ceiling during the building walkdown.

Since the room is normally unoccupied the fire will be detected by the smoke detectors observed during the building walkdown and the sprinkler system activating. The design fire is assumed to start within one of the switchgears. In the absence of specific information, the design fire will be approximated as a large electrical cabinet fire with a heat release rate of 1300 kW (this is equivalent to Test 24 of Table G-6 in [8.3.9]).



NUREG 1805 Example

Sample of NUREG spreadsheets used in Fire Scenario 4

CHAPTER 6. ESTIMATING THE IGNITION TIME OF A TARGET FUEL EXPOSED TO A CONSTANT RADIATIVE HEAT FLUX

Version 1805.0

The following calculations estimate time to ignition for flame spread of solid fuels exposed to a constant external radiative heat flux.

Parameters in **YELLOW CELLS** are Entered by the User.

Parameters in **GREEN CELLS** are Automatically Selected from the DROP DOWN MENU for the Material Selected.

All subsequent output values are calculated by the spreadsheet and based on values specified in the input parameters.

This spreadsheet is protected and secure to avoid errors due to a wrong entry in a cell(s).

The chapter in the NUREG should be read before an analysis is made.



INPUT PARAMETERS

MATERIAL FLAME SPREAD PROPERTIES

Material Flux Time Product (FTP)

Material Critical Heat Flux for Ignition ($q''_{critical}$)

Flux Time Product Index (n)

Exposure or External Radiative Heat Flux (q''_e)

| | |
|------------------|---------------------------------------|
| 42025.00 | (kW-sec/m ²) ⁿ |
| 10.00 | kW/m ² |
| 2.00 | |
| 31.00 | kW/m ² |
| Calculate | |

FLAME SPREAD PROPERTIES OF COMMON MATERIALS

| Materials | Flux Time Product (FTP) (kW-sec/m ²) ⁿ | Critical Heat Flux for Ignition $q''_{critical}$ (kW/m ²) | Flux Time Product Index, n |
|--------------------------------|--|--|-------------------------------|
| Chipboard | 5.370 | 0.4 | 1.40 |
| Chipboard (Horizontal) (15 mm) | 0.021 | 0.0 | 1.70 |
| Chipboard (Vertical) (15 mm) | 11.071 | 10.0 | 1.70 |
| Fiberboard | 3.081 | 0.3 | 1.66 |
| Hardboard | 8.127 | 0.1 | 1.40 |
| Hardboard (Painted Gloss) | 0.332 | 0.1 | 1.51 |
| Hardwood | 2.818 | 0.1 | 1.50 |
| Plywood | 8.194 | 10.0 | 1.51 |
| Plywood (Horizontal) (12 mm) | 8.409 | 0.5 | 1.50 |
| Plywood (Vertical) (12 mm) | 42.025 | 10.0 | 2.00 |
| Plywood (Painted Gloss) | 0.761 | 13.4 | 1.50 |
| PMMA (cast) (3 mm) | 3.100 | 5.0 | 1.25 |
| PMMA (extruded) (2 mm) | 1.200 | 0.0 | 1.00 |
| Polyethylene (2 mm) | 2.220 | 12.5 | 1.00 |
| Polypropylene (2.3 mm) | 8.110 | 0.5 | 1.50 |
| PVC (Extruded Gray) (3 mm) | 5.130 | 16.0 | 1.50 |
| PVC (Pressed White) (3 mm) | 95.000 | 0.0 | 2.00 |
| Softwood | 8.130 | 13.7 | 1.53 |
| Softwood (Horizontal) (20 mm) | 44.070 | 10.0 | 2.20 |
| Softwood (Vertical) (20 mm) | 16.502 | 12.0 | 1.90 |
| Softwood Intumescent Paint | 4.500 | 13.0 | 1.50 |
| User Specified Value | Enter Value | Enter Value | Enter Value |

Select Material

Flywood (Vertical) (12 mm)

Scroll to desired material then
Click on selection

Reference: SFPE Engineering Guide, "Flame Ignition of Solid Materials Under Radiant Exposure," 2002, Page 20

METHOD OF TOAL, SILCOCK AND SHIELDS

THERMALLY THICK MATERIALS

Reference: SFPE Engineering Guide, "Flame Ignition of Solid Materials Under Radiant Exposure," 2002, Page 17

$$t_{ig} = FTP_n / (q''_e - q''_{critical})^n$$

Where

t_{ig} = material ignition time (sec)

FTP_n = flux time product (kW-sec/m²)ⁿ for the given index

q''_e = exposure or external heat flux (kW/m²)

$q''_{critical}$ = material critical heat flux for ignition (kW/m²)

n = flux time product index (n > 1)

$$t_{ig} = FTP_n / (q''_e - q''_{critical})^n$$

| | | | |
|------------|-----------|-------------|--------|
| t_{ig} = | 55.29 sec | 1.55 minute | Answer |
|------------|-----------|-------------|--------|



NUREG 1805 Example

CHAPTER 9. ESTIMATING CENTERLINE TEMPERATURE OF A BUOYANT FIRE PLUME

Version 1805.0

The following calculations estimate the centerline plume temperature in a convective fire. Parameters should be specified ONLY IN THE YELLOW INPUT PARAMETER BOXES.

All subsequent output values are calculated by the spreadsheet and based on values specified in the input parameters. This spreadsheet is protected and secure to avoid errors due to a wrong entry in a cell(s). The chapter in the NUREG should be read before an analysis is made.



INPUT PARAMETERS

| | | | |
|--|---------|----------------|---------------------|
| Heat Release Rate of the Fire (Q) | 1300.00 | kW | |
| Elevation Above the Fire Source (z) | 6.00 | m | 1.93 m |
| Area of Combustible Fuel (A _c) | 15.00 | m ² | 1.39 m ² |
| Ambient Air Temperature (T _a) | 77.00 | °F | 25.00 °C |
| | | | 298.00 K |
| Calculate | | | |

AMBIENT CONDITIONS

| | | |
|--|------|--------------------|
| Specific Heat of Air (c _p) | 1.00 | kJ/kg-K |
| Ambient Air Density (ρ _a) | 1.18 | kg/m ³ |
| Acceleration of Gravity (g) | 9.81 | m/sec ² |
| Convective Heat Release Fraction (C _c) | 0.70 | |

Note: Air density will automatically correct with Ambient Air Temperature (T_a) Input

ESTIMATING PLUME CENTERLINE TEMPERATURE

Reference: NFPA Handbook of Fire Protection Engineering, 3rd Edition, 2002, Page 2-4

$$T_{\text{plume}} - T_a = 0.1 (T_a / g \cdot c_p \cdot \rho_a)^{1/3} Q_c^{2/3} (z - z_0)^{-5/3}$$

Where

- T_{plume} = plume centerline temperature (°C)
- Q_c = convective portion of the heat release rate (kW)
- T_a = ambient air temperature (K)
- g = acceleration of gravity (m/sec²)
- c_p = specific heat of air (kJ/kg-K)
- ρ_a = ambient air density (kg/m³)
- z = distance from the top of the fuel package to the ceiling (m)
- z_0 = hypothetical virtual origin of the fire (m)

Convective Heat Release Rate Calculation

$$Q_c = C_c Q$$

Where

- Q_c = convective portion of the heat release rate (kW)
- Q = heat release rate of the fire (kW)
- C_c = convective heat release fraction
- $Q_c = 910$ kW

Fire Diameter Calculation

$$A_c = D^2/4$$

Where

- A_c = area of combustible fuel (m²)
- D = fire diameter (m)
- $D = 7(4 A_c)^{1/2}$
- $D = 1.33$ m

Hypothetical Virtual Origin Calculation

$$z_0/D = -1.02 + 0.583 (Q_c^{2/3})/D$$

Where

- z_0 = virtual origin of the fire (m)
- Q_c = heat release rate of fire (kW)
- D = fire diameter (m)
- $z_0/D = 0.08$
- $z_0 = 0.10$ m

Centerline Plume Temperature Calculation

$$T_{\text{plume}} - T_a = 0.1 (T_a / g \cdot c_p \cdot \rho_a)^{1/3} Q_c^{2/3} (z - z_0)^{-5/3}$$

Where

- $T_{\text{plume}} - T_a = 958.56$
- $T_{\text{plume}} = 1256.56$ K

$T_{\text{plume}} = 958.56$ °C 1802.41 °F **Answer**



NUREG 1805 Example

CHAPTER 10. ESTIMATING SPRINKLER RESPONSE TIME Version 1805.0

The following calculations estimate sprinkler activation time:

Parameters in **YELLOW CELLS** are Entered by the User.

Parameters in **GREEN CELLS** are Automatically Selected from the DROP DOWN MENU for the Sprinkler Selected.

All subsequent output values are calculated by the spreadsheet and based on values specified in the input parameters. This spreadsheet is protected and secure to avoid errors due to a wrong entry in a cell(s). The chapter in the NUREG should be read before an analysis is made.



INPUT PARAMETERS

| | | |
|--|----------------------------|----------|
| Heat Release Rate of the Fire (Q) (Steady State) | 1300.00 kW | |
| Sprinkler Response Time Index (RTI) | 130 (m-sec) ^{1/2} | |
| Activation Temperature of the Sprinkler (T _{activation}) | 165 °F | 73.89 °C |
| Height of Ceiling above Top of Fuel (H) | 8.00 ft | 2.44 m |
| Radial Distance to the Detector (r) **never more than 0.707 or 1/2?? of the listed spacing** | 8.00 ft | 2.44 m |
| Ambient Air Temperature (T _a) | 77.00 °F | 25.00 °C |
| | | 298.00 K |
| Convective Heat Release Rate Fraction (α _c) | 0.70 | |
| r/H = | 1.33 | |
| | Calculate | |

GENERIC SPRINKLER RESPONSE TIME INDEX (RTI)**

| | | |
|------------------------|--|--|
| Common Sprinkler Type | Generic Response Time Index (RTI) (m-sec) ^{1/2} | Select Type of Sprinkler |
| Standard response bulb | 235 | Standard response link |
| Standard response link | 130 | Scroll to desired sprinkler type then Click on selection |
| Quick response bulb | 42 | |
| Quick response link | 34 | |
| User Specified Value | Enter Value | |

Reference: Madrzykowski, D., "Evaluation of Sprinkler Activation Prediction Methods" ASIAFLAM'05, International Conference on Fire Science and Engineering, 1st Proceeding, March 15-16, 1995, Kowloon, Hong Kong, pp. 215-218.

*Note: The actual RTI should be used when the value is available.

GENERIC SPRINKLER TEMPERATURE RATING (T_{activation})**

| | | | |
|----------------------------|-----------------------------------|----------------------------------|---|
| Temperature Classification | Range of Temperature Ratings (°F) | Generic Temperature Ratings (°F) | Select Sprinkler Classification |
| Ordinary | 135 to 170 | 165 | Ordinary |
| Intermediate | 175 to 225 | 212 | Scroll to desired sprinkler class then Click on selection |
| High | 250 to 300 | 275 | |
| Extra high | 325 to 375 | 350 | |
| Very extra high | 400 to 475 | 450 | |
| Ultra high | 500 to 575 | 550 | |
| Ultra high | 650 | 550 | |
| User Specified Value | - | Enter Value | |

Reference: Automatic Sprinkler Systems Handbook, 6th Edition, National Fire Protection Association, Quincy, Massachusetts, 1994, Page 57.

*Note: The actual temperature rating should be used when the value is available.

ESTIMATING SPRINKLER RESPONSE TIME

Reference: NFPA Fire Protection Handbook, 19th Edition, 2003, Page 9-140.

$$t_{activation} = (RTI / (u_{jet})) (\ln (T_{jet} - T_a) / (T_{jet} - T_{activation}))$$

Where

- t_{activation} = sprinkler activation response time (sec)
- RTI = sprinkler response time index (m-sec)^{1/2}
- u_{jet} = ceiling jet velocity (m/sec)
- T_{jet} = ceiling jet temperature (°C)
- T_a = ambient air temperature (°C)
- T_{activation} = activation temperature of sprinkler (°C)



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Ceiling Jet Temperature Calculation

$$T_{jet} - T_a = 16.9 (Q_c)^{2/3} H^{5/3} \quad \text{for } r/H \leq 0.18$$

$$T_{jet} - T_a = 5.38 (Q_c/r)^{2/3} H \quad \text{for } r/H > 0.18$$

Where T_{jet} = ceiling jet temperature ($^{\circ}\text{C}$)
 T_a = ambient air temperature ($^{\circ}\text{C}$)
 Q_c = convective portion of the heat release rate (kW)
 H = height of ceiling above top of fuel (m)
 r = radial distance from the plume centerline to the sprinkler (m)

Convective Heat Release Rate Calculation

$$Q_c = \epsilon_c Q$$

Where Q_c = convective portion of the heat release rate (kW)
 Q = heat release rate of the fire (kW)
 ϵ_c = convective heat release rate fraction

$$Q_c = 910 \text{ kW}$$

Radial Distance to Ceiling Height Ratio Calculation

$$r/H = 1.33 \quad r/H > 0.15$$

$$T_{jet} - T_a = [5.38 (Q_c/r)^{2/3}] H$$

$$T_{jet} - T_a = 152.49$$

$$T_{jet} = 177.49 \text{ (}^{\circ}\text{C)}$$

Ceiling Jet Velocity Calculation

$$u_{jet} = 0.96 (Q/H)^{1/2} \quad \text{for } r/H \leq 0.15$$

$$u_{jet} = (0.195 Q^{1/3} H^{1/2}) r^{-5/8} \quad \text{for } r/H > 0.15$$

Where u_{jet} = ceiling jet velocity (m/sec)
 Q = heat release rate of the fire (kW)
 H = height of ceiling above top of fuel (m)
 r = radial distance from the plume centerline to the sprinkler (m)

Radial Distance to Ceiling Height Ratio Calculation

$$r/H = 1.33 \quad r/H > 0.15$$

$$u_{jet} = (0.195 Q^{1/3} H^{1/2}) r^{-5/8}$$

$$u_{jet} = 1.369 \text{ m/sec}$$

Sprinkler Activation Time Calculation

$$t_{activation} = (RTI / (u_{jet})) (\ln (T_{jet} - T_a) / (T_{jet} - T_{activation}))$$

$$t_{activation} = 42.94 \text{ sec}$$

The sprinkler will respond in approximately 0.72 minutes **Answer**

NOTE: If $t_{activation} = \text{"NUM"}$ Sprinkler does not activate



NUREG 1805 Example

CHAPTER 11. ESTIMATING SMOKE DETECTOR RESPONSE TIME Version 1805.0

The following calculations estimate smoke detector response time.
Parameters should be specified ONLY IN THE YELLOW INPUT PARAMETER BOXES.
All subsequent output values are calculated by the spreadsheet and based on values specified in the input parameters. This spreadsheet is protected and sensitive to avoid errors due to a wrong entry in a cell(s).
The chapter in the NUREG should be read before an analysis is made.



INPUT PARAMETERS

Heat Release Rate of the Fire (Q) (Steady State)
Radial Distance to the Detector (r) **never more than 0.707 or 1/272 of the listed spacing**
Height of Ceiling above Top of Fuel (H)
Activation Temperature of the Smoke Detector (T_{activation})
Smoke Detector Response Time Index (RTI)
Ambient Air Temperature (T_a)

Convective Heat Release Rate Fraction (C_c)
Plume Leg Time Constant (C_{pl}) (Experimentally Determined)
Ceiling Jet Lag Time Constant (C_{cl}) (Experimentally Determined)
Temperature Rise of Gases Under the Ceiling (T_{pl})
for Smoke Detector to Activate
r/H = 1.67

| | | | |
|---------|------------------------|---------|----|
| 1300.00 | kW | 1002.17 | ft |
| 10.00 | ft | 3.05 | m |
| 6.00 | ft | 1.83 | m |
| 85.00 | °F | 30.00 | °C |
| 5.00 | (m-sec) ^{1/2} | | |
| 77.00 | °F | 25.00 | °C |
| | | 298.00 | K |
| 0.70 | | | |
| 0.67 | | | |
| 1.2 | | | |
| 18.00 | °F | 10 | °C |

Calculate

ESTIMATING SMOKE DETECTOR RESPONSE TIME METHOD OF ALPERT

Reference: NFPA Fire Protection Handbook, 19th Edition, 2007, Page 3-140
 $t_{\text{activation}} = (RTI)^2 / Q_{\text{det}} \ln \left(\frac{T_{\text{pl}} - T_a}{T_{\text{pl}} - T_{\text{activation}}} \right)$
 This method assume smoke detector is a low RTI device with a fixed activation temperature
 Where $t_{\text{activation}}$ = detector activation time (sec)
 RTI = detector response time index (m-sec)^{1/2}
 Q_{det} = ceiling jet velocity (m/sec)
 T_{pl} = ceiling jet temperature (°C)
 T_a = ambient air temperature (°C)
 $T_{\text{activation}}$ = activation temperature of detector (°C)

Ceiling Jet Temperature Calculation
 $T_{\text{pl}} - T_a = 16.9 (Q_c / r)^{0.67}$ for r/H < 0.18
 $T_{\text{pl}} - T_a = 5.38 (Q_c / r)^{0.67} / H$ for r/H > 0.18
 Where T_{pl} = ceiling jet temperature (°C)
 T_a = ambient air temperature (°C)
 Q_c = convective portion of the heat release rate (kW)
 H = height of ceiling above top of fuel (m)
 r = radial distance from the plume centerline to the detector (m)

Convective Heat Release Rate Calculation
 $Q_c = \alpha Q$
 Where Q_c = convective portion of the heat release rate (kW)
 Q = heat release rate of the fire (kW)
 α = convective heat release rate fraction
 $Q_c = 910$ kW

Radial Distance to Ceiling Height Ratio Calculation
 $r/H = 1.67$ r/H > 0.15

| | | | |
|-------|--------|-------|--------|
| >0.15 | 131.41 | <0.15 | 580.28 |
|-------|--------|-------|--------|

 $T_{\text{pl}} - T_a = 5.38 ((Q_c/r)^{0.67}) / H$
 $T_{\text{pl}} - T_a = 131.41$
 $T_{\text{pl}} = 156.41$ (°C)



NUREG 1805 Example

Ceiling Jet Velocity Calculation

$$u_{jet} = 0.98 (Q/H)^{1/3}$$

for $r/H \leq 0.15$

$$u_{jet} = (0.195 Q^{1/3} H^{1/2}) / r^{5/8}$$

for $r/H > 0.15$

Where u_{jet} = ceiling jet velocity (m/sec)
 Q = heat release rate of the fire (kW)
 H = height of ceiling above top of fuel (m)
 r = radial distance from the plume centerline to the detector (m)

Radial Distance to Ceiling Height Ratio Calculation

$$r/H = 1.67 \text{ for } r/H > 0.15$$

$$>0.15 \quad 1.14$$

$$<0.15$$

$$8.57$$

$$u_{jet} = (0.195 Q^{1/3} H^{1/2}) / r^{5/8}$$

$$u_{jet} = 1.137 \text{ m/sec}$$

Smoke Detector Response Time Calculation

$$t_{activation} = (RTI / (2u_{jet})) \ln (T_{set} - T_a) / (T_{set} - T_{activation})$$

$$t_{activation} = 0.18 \text{ sec}$$

Answer

NOTE: If $t_{activation} = \text{"NUM"}$ Detector does not activate

METHOD OF MOWRER

References: Mowrer, F., "Lag Times Associated With Fire Detection and Suppression," Fire Technology, August 1990, p. 244

$$t_{activation} = t_{pl} + t_{cj}$$

Where $t_{activation}$ = detector activation time (sec)

t_{pl} = transport lag time of plume (sec)

t_{cj} = transport lag time of ceiling jet (sec)

Transport Lag Time of Plume Calculation

$$t_{pl} = C_{pl} (H)^{4/3} / (Q)^{1/3}$$

Where t_{pl} = transport lag time of plume (sec)

C_{pl} = plume lag time constant

H = height of ceiling above top of fuel (m)

Q = heat release rate of the fire (kW)

$$t_{pl} = 0.14 \text{ sec}$$

Transport Lag Time of Ceiling Jet Calculation

$$t_{cj} = (r)^{11/8} / (C_{cj}) (Q)^{1/3} (H)^{1/2}$$

Where t_{cj} = transport lag time of ceiling jet (sec)

C_{cj} = ceiling jet lag time constant

r = radial distance from the plume centerline to the detector (m)

H = height of ceiling above top of fuel (m)

Q = heat release rate of the fire (kW)

$$t_{cj} = 0.44 \text{ sec}$$

Smoke Detector Response Time Calculation

$$t_{activation} = t_{pl} + t_{cj}$$

$$t_{activation} = 0.57 \text{ sec}$$

Answer



NUREG 1805 Example

METHOD OF MILKE

Reference: Zinke, J., "Smoke Management for Covered Mills and Mills," Fire Technology, August 1990, p. 223
 NFPA 92B, 2000 Edition, Section A.3.4 provides following correlation to estimate smoke stratification in a compartment.

$$t_{\text{activation}} = X H^{0.5} / Q^{0.17}$$

Where $t_{\text{activation}}$ = detector activation time (sec)
 $X = 4.6 \cdot 10^{-4} Y^2 + 2.7 \cdot 10^{-15} Y^5$
 H = height of ceiling above top of fuel (ft)
 Q = heat release rate from steady fire (Btu/sec)

Where $Y = T_c H^{0.5} / Q^{0.25}$
 T_c = temperature rise of gases under the ceiling for smoke detector to activate (°F)

Before estimating smoke detector response time, stratification effects can be calculated. NFPA 92B, 2000 Edition, Section A.3.4 provides following correlation to estimate smoke stratification in a compartment.

$$H_{\text{max}} = 74 Q_c^{0.25} / T_{\text{diff}}^{0.5}$$

Where H_{max} = the maximum ceiling clearance to which a plume can rise (ft)
 Q_c = convective portion of the heat release rate (Btu/sec)
 T_{diff} = difference in temperature due to fire between the fuel location and ceiling level (°F)

Convective Heat Release Rate Calculation

$$Q_c = Q \cdot \tau_c$$

Where Q_c = convective portion of the heat release rate (Btu/sec)
 Q = heat release rate of the fire (Btu/sec)
 τ_c = convective heat release rate fraction

$$Q_c = 862.52 \quad \text{Btu/sec}$$

Difference in Temperature Due to Fire Between the Fuel Location and Ceiling Level

$$T_{\text{diff}} = 1300 Q_c^{0.25} / H^{0.5}$$

Where T_{diff} = difference in temperature due to fire between the fuel location and ceiling level (°F)
 Q_c = convective portion of the heat release rate (Btu/sec)
 H = ceiling height above the fire source (ft)

$$T_{\text{diff}} = 5945.70 \quad ^\circ\text{F}$$

Smoke Stratification Effects

$$H_{\text{max}} = 74 Q_c^{0.25} / T_{\text{diff}}^{0.5}$$

$$H_{\text{max}} = 6.01 \quad \text{ft}$$

In this case the highest point of smoke rise is estimated to be 6.01 ft. Thus, the smoke would be expected to reach the ceiling mounted smoke detector.

$$Y = T_c H^{0.5} / Q^{0.25}$$

$$Y = 3.10$$

$$X = 4.6 \cdot 10^{-4} Y^2 + 2.7 \cdot 10^{-15} Y^5$$

$$X = 0.00$$

Smoke Detector Response Time Calculation

$$t_{\text{activation}} = X H^{0.5} / Q^{0.17}$$

$$t_{\text{activation}} = 0.00 \quad \text{sec} \quad \text{Answer}$$

Summary of Results

| Calculation Method | Smoke Detector Response Time (sec) |
|--------------------|------------------------------------|
| METHOD OF ALPERT | 0.18 |
| METHOD OF MOWRER | 0.57 |
| METHOD OF MILKE | 0.00 |



NUREG 1805 Example

CHAPTER 13. PREDICTING COMPARTMENT FLASHOVER HEAT RELEASE RATE Version 1805.0

The following calculations estimate the minimum heat release rate required to compartment flashover:

Parameters in **YELLOW CELLS** are Entered by the User.

Parameters in **GREEN CELLS** are Automatically Selected from the DROP-DOWN MENU for the Material Selected.

All subsequent output values are calculated by the spreadsheet and based on values specified in the input parameters. This spreadsheet is protected and secure to avoid errors due to a wrong entry in a cell(s). The chapter in the NUREG should be read before an analysis is made.



INPUT PARAMETERS

COMPARTMENT INFORMATION

Compartment Width (w_c)
 Compartment Length (L_c)
 Compartment Height (h_c)
 Vent Width (w_v)
 Vent Height (h_v)
 Interior Lining Thickness (t)
 Interior Lining Thermal Conductivity (k)

| | |
|---------|-----------|
| 20.00 | 5.096 m |
| 19.00 | 5.73 m |
| 12.00 | 3.6576 m |
| 1.50 | 0.457 m |
| 1.00 | 0.30 m |
| 0.75 | 0.01905 m |
| 0.00015 | kW/m-K |

Calculate

THERMAL PROPERTIES DATA

| Material | Thermal Conductivity k (kW/m-K) | Select Material |
|------------------------|------------------------------------|-----------------|
| Aluminum (pure) | 0.208 | Plywood |
| Steel (0.5% Carbon) | 0.054 | |
| Concrete | 0.0016 | |
| Brick | 0.0008 | |
| Glass Plate | 0.00076 | |
| Brick/Concrete Block | 0.00073 | |
| Gypsum Board | 0.00017 | |
| Plywood | 0.00012 | |
| Fiber Insulation Board | 0.00053 | |
| Chipboard | 0.00015 | |
| Aerated Concrete | 0.00026 | |
| Plasterboard | 0.00016 | |
| Calcium Silicate Board | 0.00013 | |
| Alumina Silicate Block | 0.00014 | |
| Glass Fiber Insulation | 0.000037 | |
| Expanded Polystyrene | 0.000034 | |
| User Specified Value | Enter Value | |

Scroll to desired material then Click on selection

Reference: Korte, J., J. Milke, Principles of Smoke Management, 2002, Page 270

PREDICTING FLASHOVER HEAT RELEASE RATE METHOD OF McCAFFREY, QUINTIERE, AND HARKLEROAD (MQH)

Reference: SFPE Handbook of Fire Protection Engineering, 3rd Edition, 2002, Page 3-104

$$Q_{f10} = 610 \sqrt{h_v A_T A_v} \quad (?h_v)$$

Where

Q_{f10} = heat release rate necessary for flashover (kW)
 h_v = effective heat transfer coefficient (kW/m²-K)
 A_T = total area of the compartment enclosing surface boundaries excluding area of vent openings (m²)
 A_v = area of ventilation opening (m²)
 h_v = height of ventilation opening (m)



NUREG 1805 Example

Heat Transfer Coefficient Calculation

$$h_e = k/\delta$$

Where

Assuming that compartment has been heated thoroughly before flashover, i.e., $t > t_p$.

h_e = effective heat transfer coefficient (kW/m²-K)

k = interior lining thermal conductivity (kW/m-K)

δ = interior lining thickness (m)
0.005 kW/m²-K

$$h_e =$$

Area of Ventilation Opening Calculation

$$A_v = (w_v)(h_v)$$

Where

A_v = area of ventilation opening (m²)

w_v = vent width (m)

h_v = vent height (m)

$$A_v = 0.14 \quad \text{m}^2$$

Area of Compartment Enclosing Surface Boundaries

$$A_T = [2(w_c \times l_c) + 2(h_c \times w_c) + 2(l_c \times l_c)] - A_v$$

Where

A_T = total area of the compartment enclosing surface boundaries excluding area of vent openings (m²)

w_c = compartment width (m)

l_c = compartment length (m)

h_c = compartment height (m)

A_v = area of ventilation opening (m²)

$$A_T = 157.42 \quad \text{m}^2$$

Minimum Heat Release Rate for Flashover

$$Q_{FD} = 610 \sqrt{(h_v A_T A_v)} \quad (?h_v)$$

| | | |
|------------|-----------|--------|
| $Q_{FD} =$ | 200.54 kW | Answer |
|------------|-----------|--------|

METHOD OF BABRAUSKAS

Reference: SFPE Handbook of Fire Protection Engineering, 3rd Edition, 2002, Page 3-184.

$$Q_{FD} = 750 A_v \sqrt{h_v}$$

Where

Q_{FD} = heat release rate necessary for flashover (kW)

A_v = area of ventilation opening (m²)

h_v = height of ventilation opening (m)

Minimum Heat Release Rate for Flashover

$$Q_{FD} = 750 A_v \sqrt{h_v}$$

| | | |
|------------|----------|--------|
| $Q_{FD} =$ | 57.70 kW | Answer |
|------------|----------|--------|

METHOD OF THOMAS

Reference: SFPE Handbook of Fire Protection Engineering, 3rd Edition, 2002, Page 3-184.

$$Q_{FD} = 7.8 A_T + 378 A_v \sqrt{h_v}$$

Where

Q_{FD} = heat release rate necessary for flashover (kW)

A_T = total area of the compartment enclosing surface boundaries excluding area of vent openings (m²)

A_v = area of ventilation opening (m²)

h_v = height of ventilation opening (m)

Minimum Heat Release Rate for Flashover

$$Q_{FD} = 7.8 A_T + 378 A_v \sqrt{h_v}$$

| | | |
|------------|------------|--------|
| $Q_{FD} =$ | 1256.99 kW | Answer |
|------------|------------|--------|

Summary of Results

| Calculation Method | Flashover HRR (kW) |
|----------------------|--------------------|
| METHOD OF MQH | 201 |
| METHOD OF BABRAUSKAS | 58 |
| METHOD OF THOMAS | 1257 |



NUREG 1805 Example

CHAPTER 2. PREDICTING HOT GAS LAYER TEMPERATURE AND SMOKE LAYER HEIGHT IN A ROOM FIRE WITH NATURAL VENTILATION COMPARTMENT WITH THERMALLY THICK/THIN BOUNDARIES Version 1805.0



Equation calculations estimate the hot gas layer temperature and smoke layer height in enclosure fire. Parameters in **YELLOW CELLS** are Entered by the User. Parameters in **GREEN CELLS** are Automatically Selected from the DROP-DOWN MENU for the Material Selected. All subsequent output values are calculated by the spreadsheet and based on values specified in the input parameters. This spreadsheet is protected and secure to avoid errors due to a wrong entry in a cell(s). The chapter in the NUREG should be read before an analysis is made.

INPUT PARAMETERS

COMPARTMENT INFORMATION

| | | |
|-----------------------------------|----------|-----------|
| Compartment Width (w_c) | 20.00 ft | 6.096 m |
| Compartment Length (l_c) | 19.00 ft | 5.791 m |
| Compartment Height (h_c) | 12.00 ft | 3.658 m |
| Vent Width (w_v) | 1.50 ft | 0.457 m |
| Vent Height (h_v) | 1.00 ft | 0.305 m |
| Top of Vent from Floor (V_t) | 8.00 ft | 2.438 m |
| Interior Lining Thickness (l) | 0.75 in | 0.01905 m |

AMBIENT CONDITIONS

| | | |
|-----------------------------------|------------------------|---------------|
| Ambient Air Temperature (T_a) | 77.00 °F | 25.00 °C |
| Specific Heat of Air (c_p) | 1.00 Btu/lb-K | 209.00 J/kg-K |
| Ambient Air Density (ρ_a) | 1.18 kg/m ³ | |

THERMAL PROPERTIES OF COMPARTMENT ENCLOSING SURFACES FOR

| | |
|---|---|
| Interior Lining Thermal Inertia ($k \cdot c$) | 0.16 Btu/m ² -ft ² -sec |
| Interior Lining Thermal Conductivity (k) | 0.00012 Btu/m-K |
| Interior Lining Specific Heat (c) | 0.5 Btu/lb-K |
| Interior Lining Density (ρ) | 580 kg/m ³ |

Note: Air density will automatically correct with Ambient Air Temperature (T_a) Input

EXPERIMENTAL THERMAL PROPERTIES FOR COMMON INTERIOR LINING MATERIALS

| Material | $k \cdot c$ (kW/m ² -K) ² -sec | k (kW/m-K) | ρ (kg/kg-K) | (kg/m ³) | Select Material Plywood |
|------------------------|---|-----------------|---------------------|----------------------|----------------------------|
| Aluminum (pure) | 500 | 0.206 | 0.585 | 2710 | |
| Steel (0.5% Carbon) | 197 | 0.054 | 0.405 | 7850 | |
| Concrete | 2.0 | 0.0016 | 0.75 | 2400 | |
| Brick | 1.7 | 0.0008 | 0.8 | 2000 | |
| Glass, Plate | 1.0 | 0.00076 | 0.8 | 2710 | |
| Brick/Concrete Block | 1.2 | 0.00073 | 0.84 | 1900 | |
| Gypsum Board | 0.18 | 0.00017 | 1.1 | 950 | |
| Plywood | 0.16 | 0.00012 | 2.5 | 540 | |
| Fiber Insulation Board | 0.16 | 0.00053 | 1.25 | 240 | |
| Chipboard | 0.15 | 0.00015 | 1.25 | 800 | |
| Aerated Concrete | 0.12 | 0.00028 | 0.96 | 500 | |
| Plasterboard | 0.12 | 0.00010 | 0.54 | 950 | |
| Calcium Silicate Board | 0.095 | 0.00013 | 1.12 | 700 | |
| Alumina Silicate Block | 0.035 | 0.00014 | 1 | 260 | |
| Glass Fiber Insulation | 0.0018 | 0.000037 | 0.8 | 60 | |
| Expanded Polystyrene | 0.001 | 0.000034 | 1.5 | 20 | |
| User-Specified Value | Enter Value | Enter Value | Enter Value | Enter Value | |

Reference: Peck, J., J. Milie, Principles of Smoke Management, 2002, Page 273

FIRE SPECIFICATIONS

| | |
|--------------------------------------|------------|
| Fire Heat Release Rate (\dot{Q}) | 1300.00 kW |
| Calculate | |



NUREG 1805 Example

METHOD OF McCAFFREY, GUINTIERE, AND HARKLEROD (MGH)

Reference: *Fire Handbook of Fire Protection Engineering*, 2nd Edition, 2002, page 3-178

$$\Delta T_u = 0.85 [Q^2 / (A_v (h_v)^3)]^{1/4} (A_1 h_v)^{1/5}$$

Where $\Delta T_u = T_u - T_a =$ upper layer gas temperature rise above ambient (K)
 $Q =$ heat release rate of the fire (kW)
 $A_v =$ area of ventilation opening (m²)
 $h_v =$ height of ventilation opening (m)
 $h_c =$ convective heat transfer coefficient (kW/m²-K)
 $A_1 =$ total area of the compartment enclosing surface boundaries excluding area of vent openings (m²)

Area of Ventilation Opening Calculation

$A_v = (w_v) (h_v)$
 Where $A_v =$ area of ventilation opening (m²)
 $w_v =$ vent width (m)
 $h_v =$ vent height (m)

$$A_v = 0.14 \text{ m}^2$$

Thermal Penetration Time Calculation

$t_p = (\rho c_p / k) (\Delta T)^2$
 Where $t_p =$ thermal penetration time (sec)
 $\rho =$ interior construction density (kg/m³)
 $c_p =$ interior construction heat capacity (kJ/kg-K)
 $k =$ interior construction thermal conductivity (kW/m-K)
 $\Delta T =$ interior construction thickness (m)

$$t_p = 1020.66 \text{ sec}$$

Heat Transfer Coefficient Calculation

$h_c = 7.54 (t_p)^{-1/4}$ or $h_c = 1.22 (t_p)^{-1/4}$ for $t > t_p$
 Where $h_c =$ heat transfer coefficient (kW/m²-K)
 $k \rho c_p =$ interior construction thermal inertia (kW/m²-K)²-sec
 $\Delta T =$ thermal property of material responsible for the rate of temperature rise
 $t =$ time after ignition (sec)
 See table below for results

Area of Compartment Enclosing Surface Boundaries

$A_1 = 2(w_c \times l_c) + 2(h_c \times w_c) + 2(h_c \times l_c) - A_v$
 Where $A_1 =$ total area of the compartment enclosing surface boundaries excluding area of vent openings (m²)
 $w_c =$ compartment width (m)
 $l_c =$ compartment length (m)
 $h_c =$ compartment height (m)
 $A_v =$ area of ventilation opening (m²)

$$A_1 = 157.42 \text{ m}^2$$

Compartment Hot Gas Layer Temperature With Natural Ventilation

$$\Delta T_u = 0.85 [Q^2 / (A_v (h_v)^3)]^{1/4} (A_1 h_v)^{1/5}$$

$$\Delta T_u = T_u - T_a$$

$$T_u = \Delta T_u + T_a$$

Fire results

| Time After Ignition (t) | h_c | ΔT_u | T_u | T_u | T_u | |
|-------------------------|-------|------------------------|---------|---------|---------|---------|
| (min) | (sec) | (kW/m ² -K) | (K) | (°C) | (°F) | |
| 0 | 0.00 | - | - | 258.00 | 25.00 | 77.00 |
| 1 | 60 | 0.05 | 954.08 | 1252.08 | 979.08 | 1784.37 |
| 2 | 120 | 0.04 | 1070.93 | 1368.93 | 1095.93 | 2004.68 |
| 3 | 180 | 0.03 | 1145.81 | 1433.81 | 1170.81 | 2139.45 |
| 4 | 240 | 0.03 | 1202.08 | 1500.08 | 1227.08 | 2240.75 |
| 5 | 300 | 0.02 | 1247.63 | 1545.63 | 1272.63 | 2322.74 |
| 10 | 600 | 0.02 | 1400.42 | 1698.42 | 1425.42 | 2597.75 |
| 15 | 900 | 0.01 | 1498.33 | 1796.33 | 1523.33 | 2773.99 |
| 20 | 1200 | 0.01 | 1523.79 | 1821.79 | 1548.79 | 2839.82 |
| 25 | 1500 | 0.01 | 1523.79 | 1821.79 | 1548.79 | 2839.82 |
| 30 | 1800 | 0.01 | 1523.79 | 1821.79 | 1548.79 | 2839.82 |
| 35 | 2100 | 0.01 | 1523.79 | 1821.79 | 1548.79 | 2839.82 |
| 40 | 2400 | 0.01 | 1523.79 | 1821.79 | 1548.79 | 2839.82 |
| 45 | 2700 | 0.01 | 1523.79 | 1821.79 | 1548.79 | 2839.82 |
| 50 | 3000 | 0.01 | 1523.79 | 1821.79 | 1548.79 | 2839.82 |



NUREG 1805 Example

Based on a point source radiant heat flux model presented in Appendix B, the heat flux at a specified distance can be obtained. This indicates the design fires ability to jump between fire sources, not the fires ability spread to connected fuel sources. The time to ignition of an object (plywood and polyethylene) shown in Table 7 is found using equation 7 in Appendix B. From the table below, it can be seen that plywood walls will catch fire as well adjacent switchgears are also likely to catch fire.

| Radius (m) | heat flux (kW/m ²) | Ignition time (min) | |
|------------|--------------------------------|---------------------|--------------------|
| | | Plywood (12mm) | Polyethylene (2mm) |
| 1 | 31.0 | 1.6 | 2 |
| 2 | 7.8 | will not ignite | will not ignite |
| 3 | 3.4 | will not ignite | will not ignite |
| 4 | 1.9 | will not ignite | will not ignite |
| 5 | 1.2 | will not ignite | will not ignite |

Table 7: Ignition times of plywood and polyethylene exposed to Fire Scenario 4



NUREG 1805 Example

From a fire of this size the plume temperature at 6 ft above the fuel source (assumed to be the distance to the roof) is 983°C [8.3.6] which is above the 600°C auto ignition temperature of plywood indicating that the ceiling will catch fire as a result of this design fire.

Using formulas 1-3 in Appendix B, the sprinkler activation time can be predicted. The radial distance from a sprinkler was established as 8 ft (2.4 m) which is approximated from the sprinkler plan drawing [8.2.11] since the sprinkler layout details of the active machine shop sprinkler system were unavailable. The resulting sprinkler response time is 0.72 minutes. The smoke detectors assuming a 10 ft. radial distance (exact locations could not be found on drawings) have a response time of less than 1 second, indicating they will alarm before the fire reaches its full size.

Flashover is associated with a hot gas layer temperature of 600°C. Using the methods predicted in NUREG 1805 [8.3.6], the minimum required heat flux will be reached. The minimum required heat fluxes using the three provided methods are 201, 58 and 1257 kW. The same result is obtained using a natural ventilation model and predicting the hot gas layer temperature. It can be concluded that flashover will occur in this compartment as a result of a fire of this size, excluding sprinkler response.



NUREG 1805 Example

Fire spread to adjacent compartments is considered unlikely since plywood walls can be assigned a fire resistance rating of at least 10 minutes according to D-2.3.4.A of the building code [8.1.1]. Since there is a sheet of plywood on each side of the wall this give the wall a fire resistance rating of approximately 20 minutes. This is approximately double the time it will take the fire department to respond.

Area 135

| Combustible Type | Units of Measure | Heat of Combustion (Btu/Unit) | Combustible Load (kg/Unit) | Quantity | Contribution (BTU) | Contribution (kg) |
|-----------------------------|------------------|-------------------------------|----------------------------|----------|--------------------|-------------------|
| Power Cord - 1/2" Diameter | Feet | 366 | 0.034405 | 2750 | 1.01E+06 | 9.46E+01 |
| Rubber Hose - 1/2" Diameter | Feet | 1170 | 0.027656 | 20 | 2.34E+04 | 5.53E-01 |
| Fluorescent Light Fixture | Fixture(s) | 19800 | 1 | 2 | 3.96E+04 | 2.00E+00 |

Total Combustible Load
1.07E+06 BTU
1.01E+06 kJ
9.72E+01 kg



Agenda:

Introduction

NUREG 1805 Example

Group Example



Group Example

- The room has approximate LxWxH dimension of 19 x 20 x 12 ft (5.8 x 6.1 x 3.6 m).
- A small non-mechanical vent with dimensions 18 x 12 inches (Natural ventilation) and top of vent from floor is 8 ft or 2.438m.
- Interior lining thickness 0.75 inch or 0.019m
- The walls and roof of the room are of wooden construction.(Plywood 12mm)
- The combustibles in the room are comprised of electrical equipment and 3 cables.
- Area of combustibles is 1.39 m².



Group Example

Using NUREG 1805 spread-sheet, Calculate:

- The heat release rate (HRR)?
- The centreline temperature of the plume at 6ft or 1.83m?
- The smoke detector response time? (with radial distance from the detector of 10ft or 3.05m and room temperature 25C)
- The ignition time of target fuel from radiant heat flux?
- Smoke layer height?





Thank you
Questions?



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